

Homework 1

- 1) For the screw extruders shown on page 5 figure 1.3 explain what the various arrangements of screw threads might be achieving in a processing application.
Why is a rubber extruder shorter than a thermoplastic extruder? (Refer to figures 12.1 pp. 468, 12.7 pp. 477 and 17.1 pp. 685)
- 2) Most injection molding processes involve a two-step injection into the mold. Besides empirical approaches explain what guidelines you might use to design a protocol for this two step process (pp. 11, section 14.1 pp. 584). Explain the terms: hold time, gate, shot, soak, parting line, flash, fan, runner, front region, and weld line for an injection molding machine.
- 3) The entanglement molecular weight (fig. 2.3) defines the limit of useful properties in a polymer, e.g. PS below 10k is brittle. Explain how this is determined and why it varies for different polymers. Why do properties differ above and below the entanglement molecular weight?
- 4) Materials with $D_e = 0$ and $D_e = 15$ have different properties. Explain these. How is "time-temperature" superposition related to the D_e approach? Why are "time-temperature superposition" and the Deborah number important to processing? (pp. 40, 163)

Answers Homework 1

1)

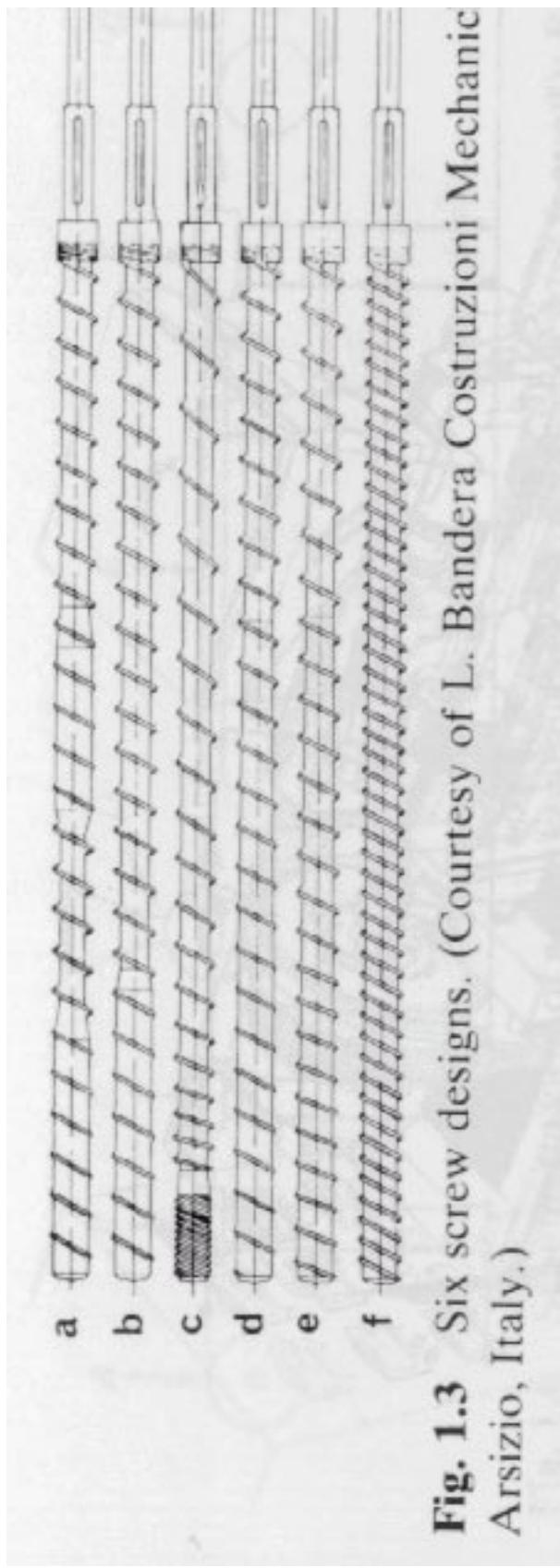


Fig. 1.3 Six screw designs. (Courtesy of L. Bandera Costruzioni Mechanic Arsizio, Italy.)

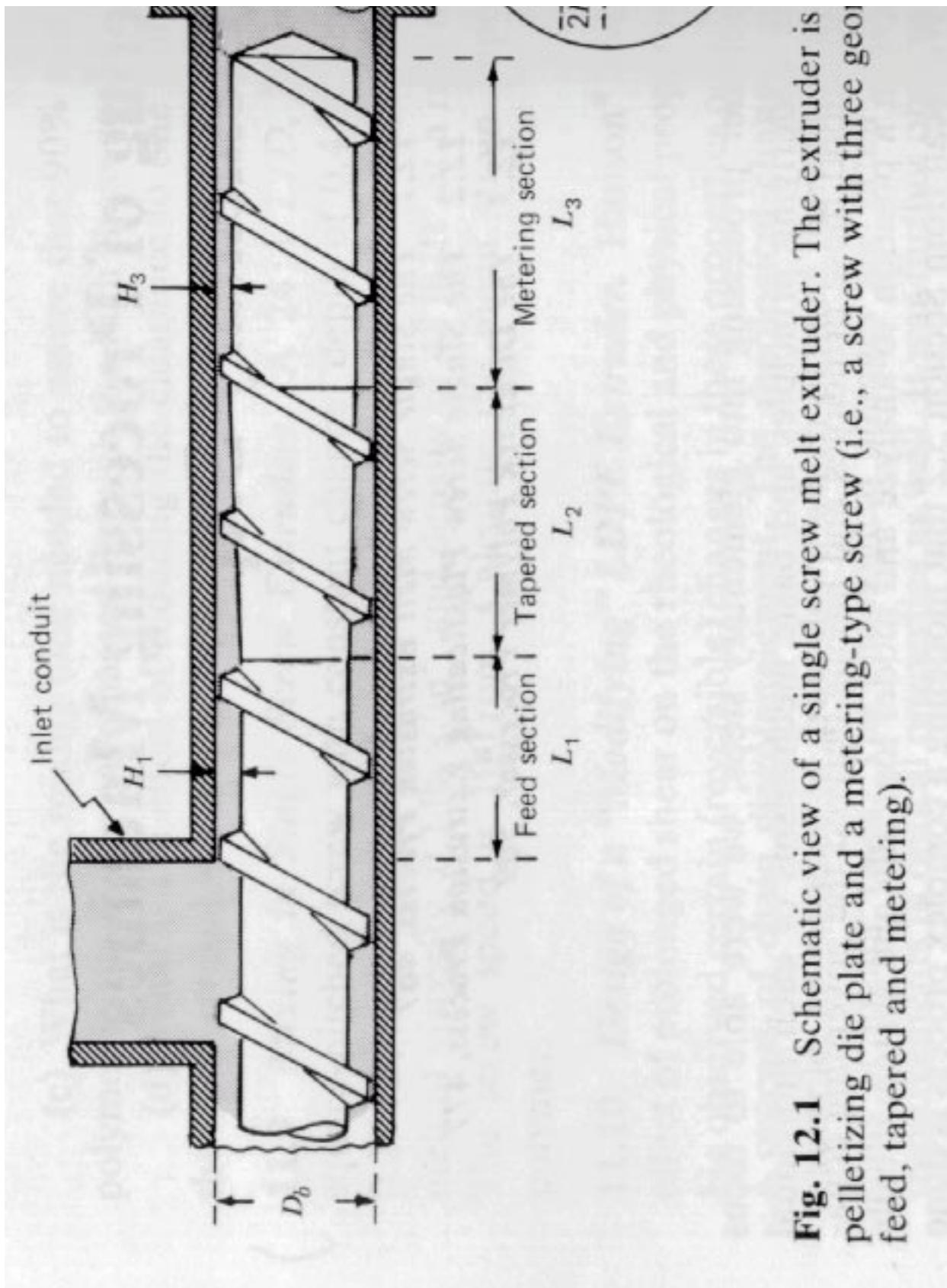


Fig. 12.1 Schematic view of a single screw melt extruder. The extruder is pelletizing die plate and a metering-type screw (i.e., a screw with three geometric feed, tapered and metering).

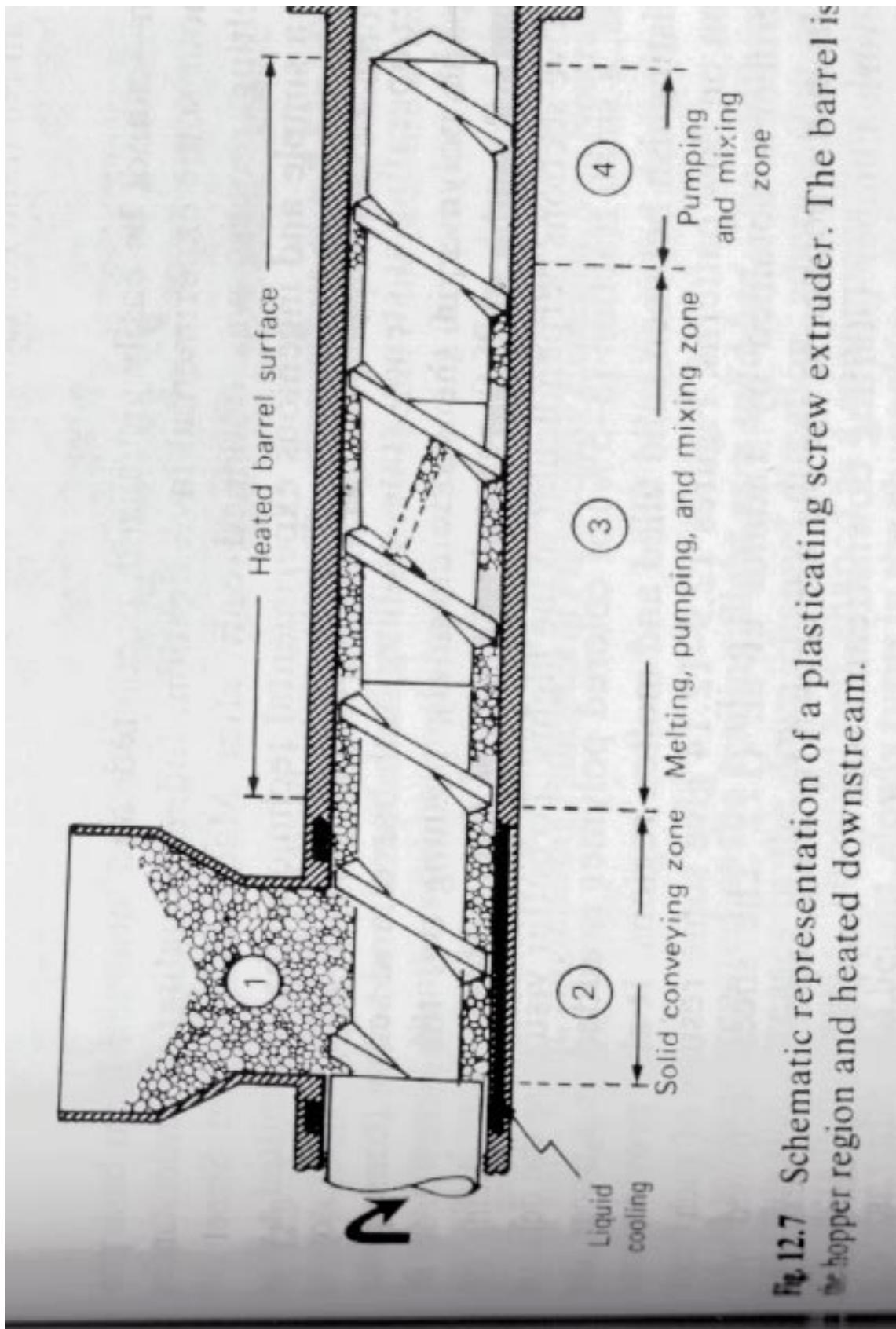
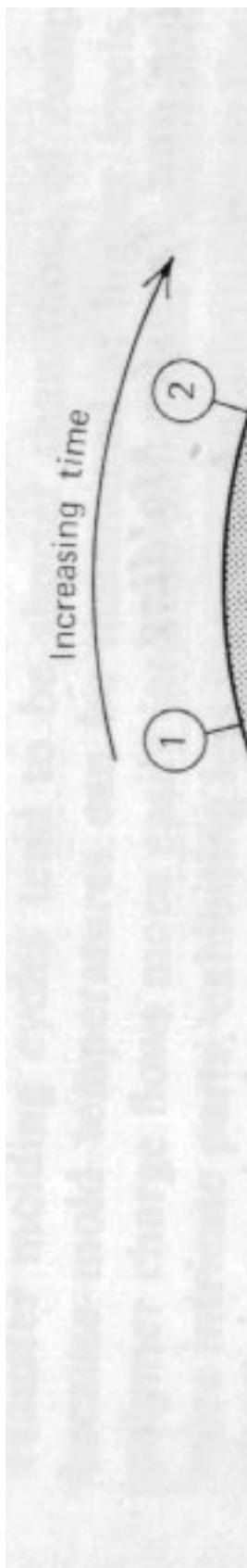


Fig. 12.7 Schematic representation of a plasticating screw extruder. The barrel is
the hopper region and heated downstream.



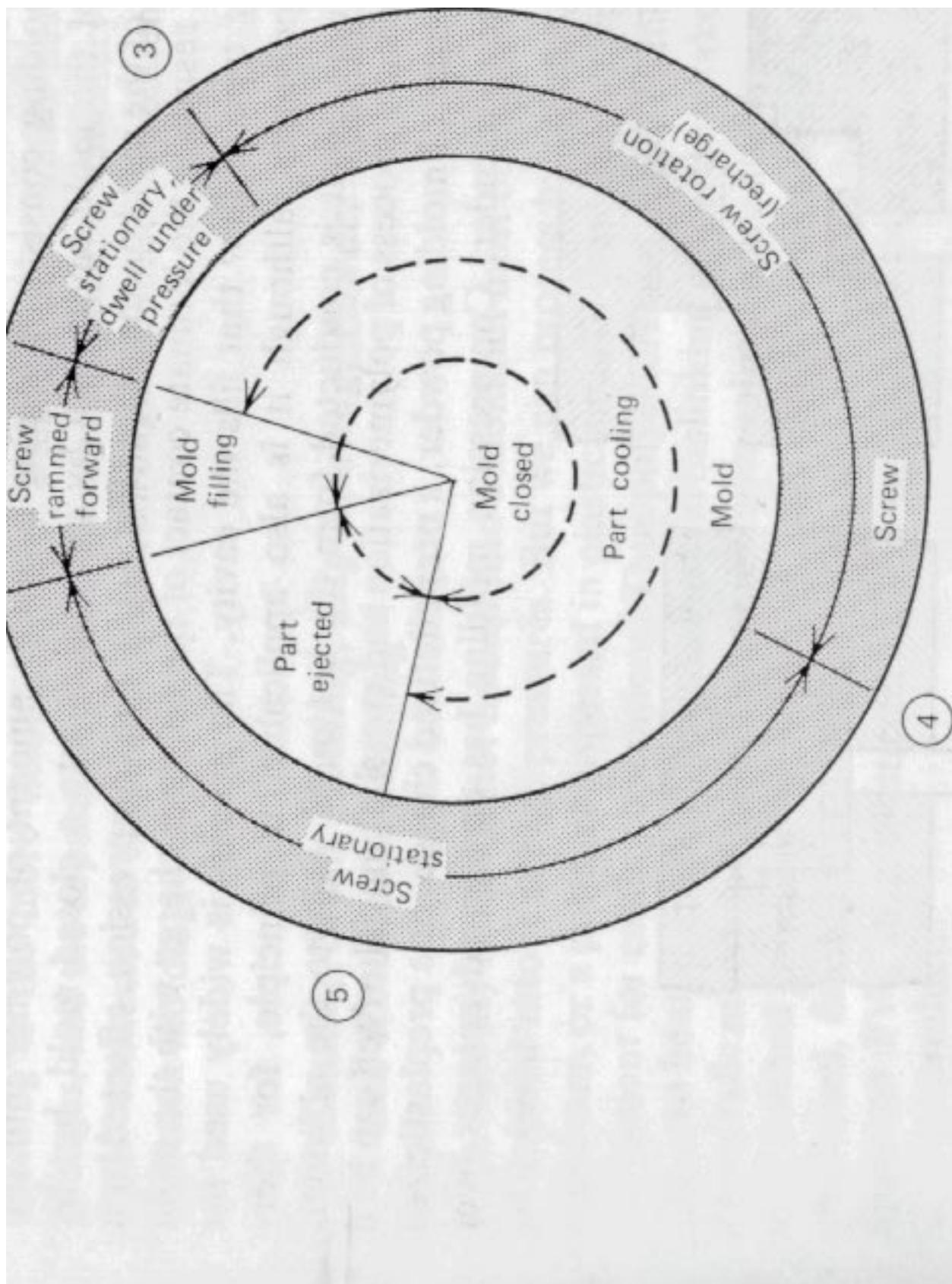


Fig. 1.13 The injection molding cycle. [Reprinted with permission from *Polym. Eng. Sci.*, **11**, 353 (1971).]

